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(54) Title: PROCESS FOR PRODUCING SILANE-CROSSLINKED POLYOLEFIN

(57) Abstract

A process for producing a silane-crosslinked polyolefin which is characterized by melt-blending (i) a polyolefinic base polymer, (ii) a carrier polymer A containing an organic unsaturated silane and a free radical generating agent and containing substantially no water and (iii) a carrier polymer B containing a silanol condensation catalyst and an antioxidant, at a temperature higher than the crystal melting point of the base polymer to effect reaction, and then contacting the resulting reaction product with water to effect crosslinking. The process can provide a silane-crosslinked polyolefin excellent in extrusion processability as well as in crosslinking property, mechanical property and heat resistance.

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DESCRIPTION

PROCESS FOR PRODUCING SILANE-CROSSLINKED POLYOLEFIN

Technical Field

The present invention relates, in the silanecrosslinking of polyolefins, a process of silanecrosslinking for producing a silane-crosslinked
polyolefin in one step which uses a carrier polymer A
containing an organic unsaturated silane and the like
in a high concentration and a carrier polymer B
containing a silanol condensation catalyst and the
like.

10 Background Art

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A simple method which has been widely known for crosslinking polyolefins is the so-called silane crosslinking method which comprises grafting an organic unsaturated silane to the polyolefin in the presence of a free radical generating agent to effect silane grafting, and then contacting the resulting silane-grafted polymer with water in the presence of a silanol condensation catalyst to effect crosslinking. This method is disclosed, for example, in JP-B-48-1711 and JP-A-57-49109.

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However, this method comprises at least two steps, that is, the silane grafting step and the silanol condensation step. Accordingly, at least two extrusion steps are necessary to obtain the ultimate product, inevitably resulting in economical disadvantage.

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An already known one-step process is the monosil process. This process requires a liquid addition apparatus for injecting an organic unsaturated silane in the form of liquid into an extruder, and hence involves the problems of slippage and metering error. Moreover, the process requires an expensive special type extruder with a high L/D ratio to insure uniform dispersion of small amounts of additives, resulting in economical disadvantage. Furthermore, a very high grade technique is necessary in the extrusion.

Another known one-step process is a silane crosslinking method which introduces silane into a solid carrier polymer disclosed in JP-A-3-167229. In this method, however, a porous polymer or EVA is used as the solid carrier polymer and, in addition to silane and a free radical generating agent, such other additives as a silanol condensation catalyst and an antioxidant are introduced to the solid carrier polymer; hence the method involves the problems of low crosslinking efficiency and poor storability caused by oligomerization by condensation of silane or inhibition

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of crosslinking due to radical capture.

The present invention has been made to overcome the aforesaid problems and has for its object to provide, in the silane-crosslinking of polyolefins, a process of silane-crosslinking for producing a silane-crosslinked polyolefin in one step which uses a carrier polymer A containing an organic unsaturated silane and the like in high concentrations and a carrier polymer B containing a silanol condensation catalyst and the like.

Disclosure of the Invention

The present invention relates to a process for producing a silane-crosslinked polyolefin which is characterized by melt-blending (i) a polyolefinic base polymer, (ii) a carrier polymer A containing an organic unsaturated silane represented by the formula RR'SiY2, wherein R is a monovalent olefinic unsaturated hydrocarbon group, Y is a hydrolyzable organic group, and R' is a monovalent hydrocarbon group other than aliphatic unsaturated hydrocarbon groups or is the same group as Y, and a free radical generating agent and containing substantially no water and (iii) a carrier polymer B containing a silanol condensation catalyst and an antioxidant, at a temperature higher than the crystal melting point of the base polymer to effect reaction, and then contacting the resulting reaction product with water to effect crosslinking. In this process for

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producing a silane-crosslinked polyolefin, the base polymer is preferably a polymer selected from the group consisting of polyethylene, polypropylene, copolymer of ethylene and an α -olefin, ethylene-ethyl acrylate copolymer (EEA), ethylene-methyl methacrylate copolymer 5 (EMMA), ethylene-vinyl acetate copolymer (EVA), chlorinated polyethylene (CPE), and the mixtures thereof; the carrier polymer A is preferably a polymer selected from the group consisting of ethylene-ethyl 10 acrylate copolymer (EEA), ethylene-methyl methacrylate copolymer (EMMA), a hydrogenated block copolymer obtained by hydrogenating a block copolymer consisting essentially of a polymer block comprising at least one vinylaromatic compound as the principal monomer unit 15 and a polymer block comprising at least one conjugated diene compound as the principal monomer unit, and the mixtures thereof; the carrier polymer B is preferably a polymer selected from the group consisting of polyethylene, polypropylene, copolymer of ethylene and an 20 α -olefin, and the mixtures thereof; and the total amount of the carrier polymer A and the carrier polymer B is preferably 3-15% by weight.

Best Mode for Carrying Out the Invention

The present invention is described in detail
below.

The polyolefinic base polymer used in the present invention is not particularly limited and may

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be, for example, common polyethylene, polypropylene, copolymer of ethylene and an α -olefin (wherein the α -olefin may be C_3 - C_{12} α -olefins, e.g., propylene, butene-1, pentene-1, octene-1, 4-methylpentene-1, 4-methylhexene-1, 4,4-dimethylpentene-1, nonene-1, decene-1, undecene-1 and dodecene-1), ethylene-ethyl acrylate copolymer (EEA), ethylene-methyl methacrylate copolymer (EMMA), ethylene-vinyl acetate copolymer (EVA), chlorinated polyethylene (CPE), and the mixtures thereof.

The organic unsaturated silane used in the present invention is grafted to the base resin to serve as the point which crosslinks the base resin molecules with each other. The organic unsaturated silane used in the present invention is a compound represented by the formula RR'SiY2, wherein R is a monovalent olefinic unsaturated hydrocarbon group, Y is a hydrolyzable organic group, R' is a monovalent hydrocarbon group other than aliphatic unsaturated hydrocarbon groups or is the same group as Y. Preferably used is an organic unsaturated silane in which R' and Y are the same and which is represented by the formula RSiY3, for example, vinyltrimethoxysilane, vinyltriethoxysilane, vinyltributoxysilane, allyltrimethoxysilane and allyltriethoxysilane.

The amount of the organic unsaturated silane to be added is 0.1-5% by weight, preferably 0.7-3% by weight, based on the total weight of polymers. When

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the amount is less than 0.1% by weight, a sufficient grafting do s not take place. An amount larger than 5% by weight may cause defective molding and also is economically disadvantageous.

5 The free radical generating agent used in the present invention acts as the initiator of silane grafting. The free radical generating agent used in the present invention may be various organic peroxides and peresters which have 'a strong polymerization initiating effect, for example, dicumyl peroxide, α,α' -10 bis(t-butylperoxydiisopropyl)benzene, di-t-butyl peroxide, t-butyl cumyl peroxide, dibenzoyl peroxide, 2,5-dimethyl-2,5-bis(t-butylperoxy)hexane, t-butyl peroxypivalate, and t-butyl peroxy-2-ethylhexanoate. 15 The amount of the agent to be added is 0.01-0.5% by weight, preferably 0.05-0.2% by weight, relative to the total weight of polymers. When the amount is less than 0.01% by weight, the silane grafting does not proceed sufficiently. When the amount is larger than 0.5% by 20 weight, both the extrusion processability and the

The free radical generating agent and the organic unsaturated silane can be incorporated into the carrier polymer A of the present invention by swelling the carrier polymer A with a liquid mixture obtained by dissolving the free radical generating agent in the organic unsaturated silane. For incorporating the silane into polymer to a high concentration at this

surface appearance of moldings tend to be poor.

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time, the carrier polymer A needs to be preheated, but the temperature must not be higher than the crystal melting point of the polymer lest the polymer should undergo melting.

5 The carrier polymer A must be in the form of granules and must be compatible with the base polymer to be crosslinked and with the silane. "compatible" herein means that the carrier polymer A should not readily react with the silane and should be 10 dispersible or soluble in the base polymer. suitable carrier polymer A is non-hygroscopic. the moisture absorption rate of the polymer is preferably relatively slow in order to minimize the possibility of premature hydrolysis and condensation of In any way, substantially no water should the silane. be present in the carrier polymer A. The carrier polymer A used in the present invention is usually made into the form of granules, including pellets. Preferred is the form of pellets.

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The carrier polymer A used in the present invention may be, for example, ethylene-ethyl acrylate copolymer (EEA), ethylene-methyl methacrylate copolymer (EMMA), a hydrogenated block copolymer obtained by hydrogenating a block copolymer consisting essentially of a polymer block comprising at least one vinylaromatic compound as the principal monomer unit and a polymer block comprising at least one conjugated diene compound as the principal monomer unit, e.g.,

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hydrogenated styrene-isoprene block copolymer (SEPS) and hydrogenated styrene-butadiene block copolymer (SEBS), and the mixtures thereof. Preferred of these

is EEA or EMMA.

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5 The silanol condensation catalyst, antioxidant, etc. may be incorporated into the carrier
polymer B of the present invention by kneading them
with the carrier polymer B, followed by granulation.
The carrier polymer B should be in the form of granules
and should be a solid compatible with the base polymer
to be crosslinked. The carrier polymer B is usually
made into the form of granules, including pellets.
Preferred is the form of pellets.

The carrier polymer B has a softening point equal to or higher than that of the carrier polymer A.

The carrier polymer B used in the present invention may be, for example, polyethylene, polypropylene, copolymer of ethylene and an α -olefin, wherein the α -olefin may be C_3 - C_{12} α -olefins, e.g., propylene, butene-1, pentene-1, octene-1, 4-methylpentene-1, 4-methylpentene-1, 4-dimethylpentene-1, nonene-1, decene-1, undecene-1, dodecene, and the mixtures thereof.

The silanol condensation catalyst used in the

25 present invention may be such organometallic compounds
as dibutyltin dilaurate, stannous acetate, dibutyltin
diacetate, dibutyltin dioctoate, lead naphthenate, zinc
caprylate, cobalt naphthenate, tetrabutyl titanate,

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lead stearate, zinc stearate, cadmium stearate, barium stearate and calcium stearate.

The amount of the silanol condensation catalyst to be added is 0.01-0.2% by weight, preferably 0.02-0.1% by weight, based on the total weight of polymers. When the amount is less than 0.01% by weight, the crosslinking reaction does not proceed sufficiently. When the amount is larger than 0.2% by weight, local crosslinking proceeds in the extruder at the time of extrusion, resulting in a greatly deteriorated appearance of the product. The silanol condensation catalyst should be incorporated into the carrier polymer B. This is because if the catalyst is incorporated into the carrier polymer A, oligomerization by condensation of the silane is promoted to cause deterioration of the appearance of products.

The antioxidant used in the present invention may be those conventionally used in processing polyolefins and is not particularly limited, but it should be incorporated into the carrier polymer B. This is because if it is incorporated into the carrier polymer A, crosslinking is inhibited owing to radical capture. Also when other additives are added, those additives which have the possibility of inhibiting crosslinking should be incorporated into the carrier polymer B.

The carrier polymers are added in such amounts that the sum of the amounts of the carrier polymers A and B is in the range of 3-15% by weight.

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When it is less than 3% by weight, a sufficient grafting does not take place. An amount larger than 15% causes defective molding and is at the same time economically disadvantageous.

As other additives, if necessary and desired, conventionally used additives, for example, neutralizing agents, ultraviolet absorbers, antistatic agents, pigments, dispersants, thickeners, corrosion inhibitors, mildewproofing agents, flow regulators, other inorganic fillers and other synthetic resins, may be added.

The present invention is described below with reference to Examples.

Preparation of carrier polymer A

Table 1, first a carrier polymer A was poured into a Super Mixer, mixed with stirring and preheated to 80°C. Then a liquid mixture obtained by dissolving a free radical generating agent in an unsaturated silane was poured into the Super Mixer and, while stirring, the carrier polymer A was impregnated with the liquid mixture for 10 minutes.

Preparation of carrier polymer B

According to the compounding ratio shown in

Table 2, a carrier polymer B, silanol condensation

catalyst, antioxidant, etc. were kneaded by using a

pressure kneader and granulated.

- * Materials used
 - (1) EEA: ethylene-ethyl acrylate copolymer (EA
 content: 23% by weight)
- 5 (2) SEPS: hydrogenated styrene-isoprene block copolymer (styrene content: 30% by weight)
 - (3) L-LDPE: linear low density polyethylene (density: 0.924 g/cm³, MI: 3.0 g/10 min)
 - (4) VTMOS: vinyltrimethoxysilane
- 10 (5) DCP: dicumyl peroxide
 - (6) LDPE: low density polyethylene (density:
 0.925 g/cm³, MI: 1.5 g/10 min)
 - (7) PP: polypropylene (homopolymer, MI(230°C):
 2.0 g/10 min)
- 15 (8) DBTDL: Dibutyltin dilaurate
 - (9) Antioxidant: phenolic antioxidant/Irganox 1010
 (mfd. by Ciba Geigy Corp.)
 - (10) Lubricant: low molecular weight polyethylene/ Sanwax 171P (mfd. by Sanyo Chemical Industries, Ltd.)
 - (11) MDPE: medium density polyethylene (density: 0.930 g/cm³, MI: 2.0 g/10 min)
 - * Method of evaluation

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- (12) Silane impregnability:
- Impregnability was examined by heating and stirring the objective polymer with a VTMOS/DCP liquid mixture in a Super Mixer.
 - 0 : well impregnable, x : not impregnable

- (13) Extruded tape appearance
 50 mmφ extruder, 120-150-170-180-170°C
 L/D: 20, compression ratio: 3.5
 tape die: width 100 m, lip gap 1 mm
- 5 Evaluation: Results were evaluated in the order of 0 > Δ > x, the level of 0 being judged as acceptable.
 - (14) Gel fraction (%): xylene immersion method, 120°C, 20 hours
- 10 (15) Tensile strength (MPa) and elongation (%):
 According to JIS K 6760
- A polyolefinic base polymer and the carrier polymers A and B prepared above were blended in the proportions shown in Tables 3 and 4, the blend was extruded with an extruder into a tape and the tape was immersed in warm water, to effect crosslinking. The extruded tape was evaluated for its gel fraction, tensile strength, elongation and heat distortion.

13 Table 1

Compounding ingredient	A1	A2	А3	A4	A5	A6	A7
EEA	95	100		95	95	95	95
SEPS	5			5	5	5	5
L-LDPE			100				
VTMOS .	45	40	40	100	2	45	. 45
DCP	2.16	1.92	1.92	4.8	0.5	0.2	20
Silane impregna- bility	0	0	×	×	0	0	0

Table 2

Compounding ingredient	B1	В2	в3	B4
LDPE	100		100	100
PP		100		
DBTDL	5	5	0.5	25
Antioxidant	16	16	16	16
Lubricant	5	5	5	5

14 Table 3

				T			AF
	Example		Comparative Example				
	1	2	3	1	2	3	4
<pre><compounding ingredient=""></compounding></pre>							
LDPE	93.5	B		93.5			93.5
L-LDPE		93			93.5		B
MDPE			92.5			93.5	
A1	5						5
A2] 	5.5	5.5				
A 5				5			
A6					5		
A7						5	
B1	1.5		2		1.5	1.5	
B2 .		1.5		1.6	·		
В3							1.5
<evaluation item=""></evaluation>							
Extruded tape appearance	0	0	0	×	0	×	0
Gel fraction (%)	75	74	76	5	10	80	25
Tensile strength (M Pa)	19	21	23	-	18	-	18
Elongation (%)	450	500	470	-	490	-	460
Heat defor- mation (%)	12	8	7	-	-	-	-
Overall evaluation	0	0	0	×	×	×	×

Note: Symbol - means that determination was impossible.

15 Table 4

	Comparative Example				
	5	6	7		
<compounding ingredient=""></compounding>					
LDPE		97.5			
L-LDPE	93.5				
MDPE			81.5		
A1		1			
A2	5		17		
B1		1.5			
B2			1.5		
В4	1.5				
<evaluation item=""></evaluation>					
Extruded tape appearance	×	0	×		
Gel fraction (%)	78	20	82		
Tensile strength (MPa)	-	18	-		
Elongation (%)	-	460	_		
Heat deformation (%)	1 (<u>*</u>)	1- 1 <u>-2-</u>	-		
Overall evaluation	×	×	×		

Note: Symbol - means that determination was impossible.

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As is apparent from Tables 3 and 4, the materials shown in Examples 1, 2 and 3 show good extrusion processability and quite excellent crosslinking property, mechanical property and heat resistance.

In contrast, the materials shown in Comparative Examples are all poorly balanced among extrusion processability, crosslinking property, mechanical property and heat resistance.

10 Industrial Applicability

The process of the present invention is a very useful silane crosslinking process which can provide silane-crosslinked polyolefins excellent in extrusion processability as well as in crosslinking property, mechanical property and heat resistance.

CLAIMS

- 1. A process for producing a silane-crosslinked polyolefin which is characterized by melt-blending (i) polyolefinic base polymer, (ii) a carrier polymer A containing an organic unsaturated silane represented by 5 the formula RR'SiY2, wherein R is a monovalent olefinic unsaturated hydrocarbon group, Y is a hydrolyzable organic group, and R' is a monovalent hydrocarbon group other than aliphatic unsaturated hydrocarbon groups or 10 is the same group as Y, and a free radical generating agent and containing substantially no water and (iii) a carrier polymer B containing a silanol condensation catalyst and an antioxidant, at a temperature higher than the crystal melting point of the base polymer to 15 effect reaction, and then contacting the resulting reaction product with water to effect crosslinking. 2. The process for producing a silanecrosslinked polyolefin according to claim 1 wherein the base polymer is selected from the group consisting of 20 polyethylene, polypropylene, copolymer of ethylene and an α -olefin, ethylene-ethyl acrylate copolymer (EEA), ethylene-methyl methacrylate copolymer (EMMA), ethylene-vinyl acetate copolymer (EVA), chlorinated
- 25 3. The process for producing a silanecrosslinked polyolefin according to claim 1 wherein the
 carrier polymer A is selected from the group consisting

polyethylene (CPE), and the mixtures thereof.

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of ethylene-ethyl acrylate copolymer (EEA), ethylenemethyl methacrylate copolymer (EMMA), a hydrogenated
block copolymer obtained by hydrogenating a block
copolymer consisting essentially of a polymer block
comprising at least one vinylaromatic compound as the
principal monomer unit and a polymer block comprising
at least one conjugated diene compound as the principal
monomer unit, and the mixtures thereof.

- 4. The process for producing a silane-
- crosslinked polyolefin according to claim 1 wherein the carrier polymer B is selected from the group consisting of polyethylene, polypropylene, copolymer of ethylene and an α -olefin, and the mixtures thereof.
 - 5. The process for producing a silane-
- 15 crosslinked polyolefin according to claim 1 wherein the total amount of the carrier polymer A and the carrier polymer B is 3-15% by weight.
 - 6. The process for producing a silanecrosslinked polyolefin according to claim 1 wherein the
 amount of the organic unsaturated silane added in the
 carrier polymer A is 0.1-5% by weight based on the
 total weight of the silane-crosslinked polyolefin.
- 7. The process for producing a silanecrosslinked polyolefin according to claim 1 wherein the
 25 amount of the free radical generating agent added in
 the carrier polymer A is 0.01-0.5% by weight based on
 the total weight of the silane-crosslinked polyolefin.
 - 8. The process for producing a silane-

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crosslinked polyolefin according to claim 1 wherein the amount of the silanol condensaiton catalyst added in the carrier polymer B is 0.01-0.2% by weight based on the total weight of silane-crosslinked polyolefin.

INTERNATIONAL SEARCH REPORT

Inte: onal Application No
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A. CLASS IPC 6	IFICATION OF SUBJECT MATTER C08L43/04 C08J3/22		
According	to International Patent Classification (IPC) or to both national cla	safication and IPC	
	S SEARCHED		
Minimum of IPC 6	documentation searched (classification system followed by classific COBL COBJ	cation symbols)	
Documenta	tion searched other than minimum documentation to the extent th	at such documents are included in the fields s	searched
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C. DOCUM	MENTS CONSIDERED TO BE RELEVANT		
Category *	Citation of document, with indication, where appropriate, of the	relevant passages	Relevant to claim No.
X	DE,A,31 50 808 (DIPOX KURT SCHU June 1983 see complete document	LZE KG) 30	1-8
A	EP,A,O 426 073 (UNION CARBIDE C PLASTIC) 8 May 1991 see page 3, line 10 - page 5, 1 claims 1,22		1
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A	DE,A,26 17 108 (KABEL METALLWER October 1977 see claims 1,7		1
Fwr	ther documents are listed in the continuation of box C.	Patent family members are listed	in annex.
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information on patent family members

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